



Rheological, viscoelastic and plastic properties of faecal sludge from VIP latrines

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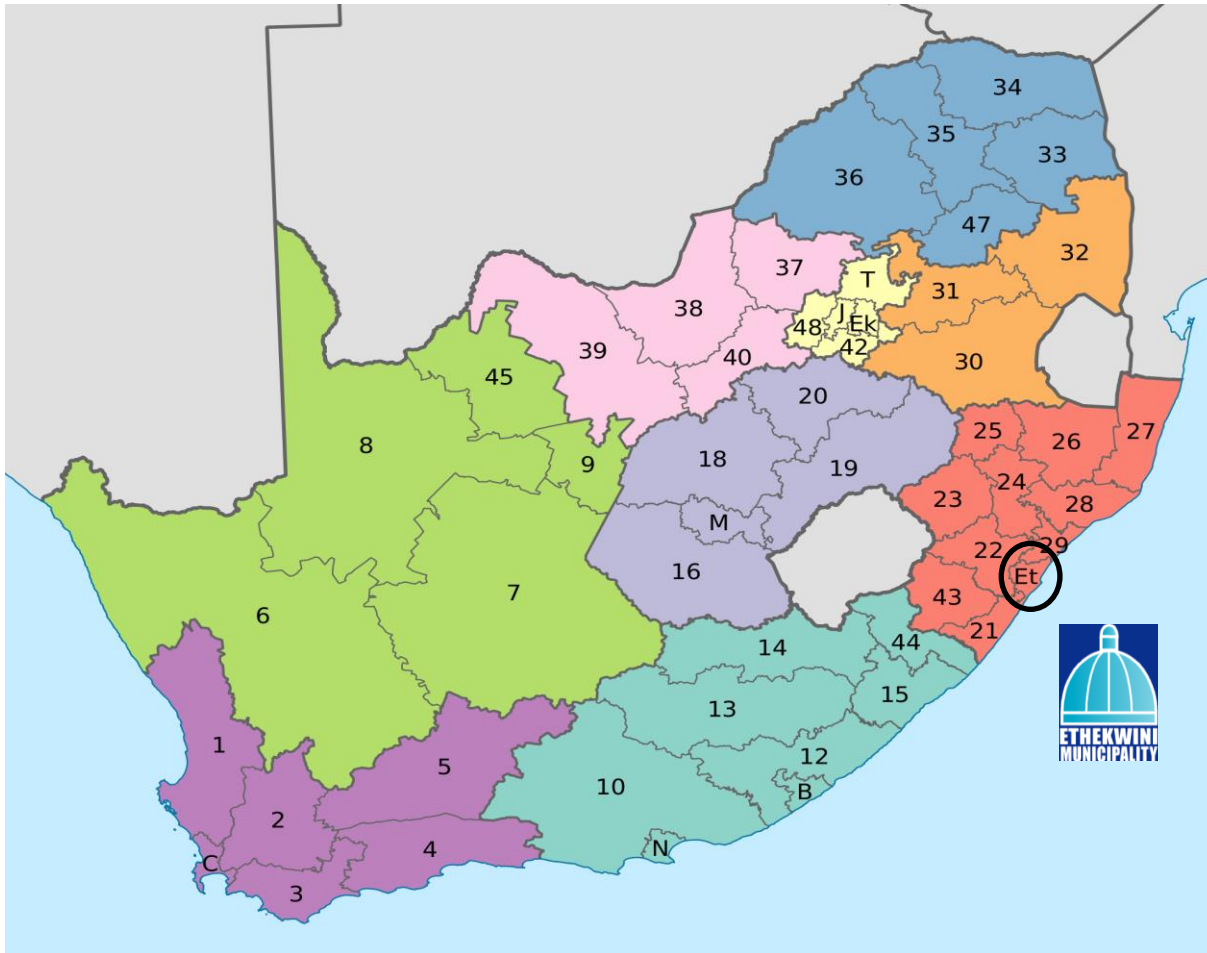
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Motivation of the study

- VIP latrines widespread worldwide, particularly in the African context
- Faecal sludge an hazardous material
- Lack of data in literature about mechanical properties of faecal sludge
- Required for the design of pit emptying, mechanical handling and process equipment



Location of the study

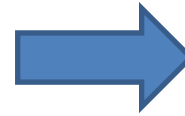
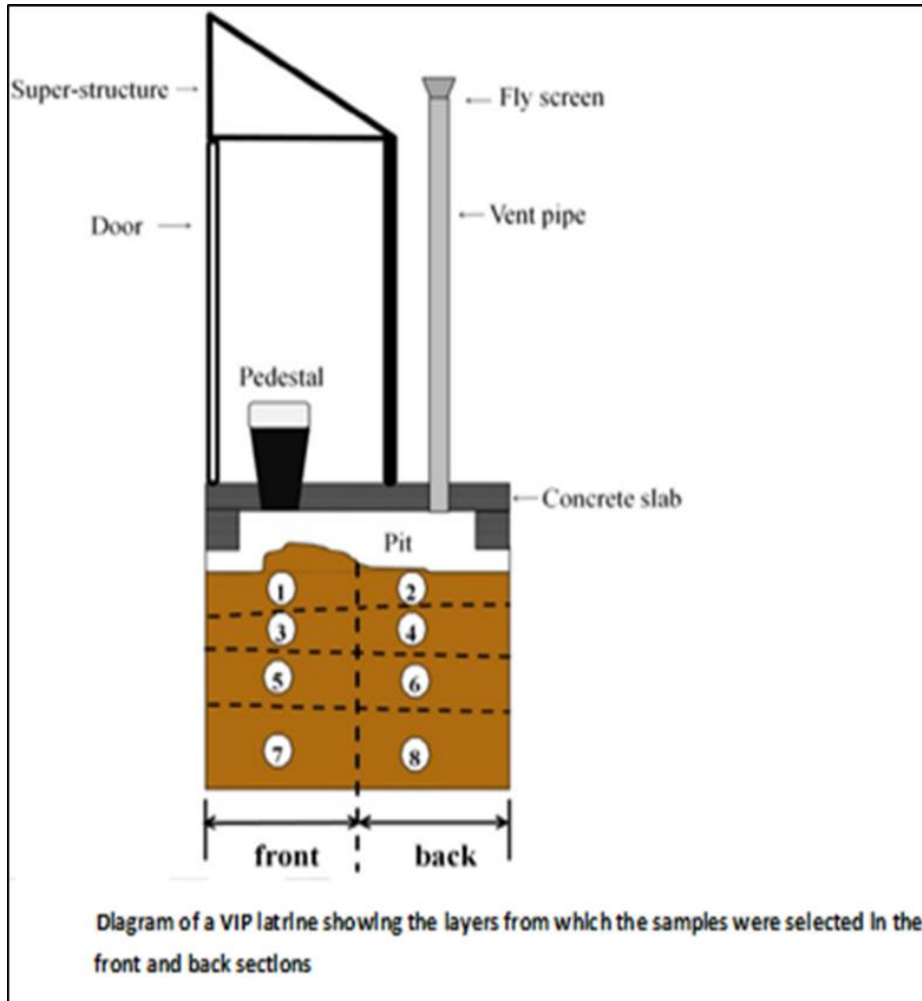


30,000 VIP latrines

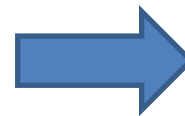


Methodology

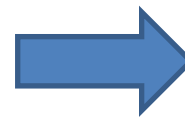
Sampling



- Rheometer:
- Static tests (flow)
 - Dynamic tests (viscoelasticity)



- Cone penetrometer:
- Liquid limit
 - Plastic limit

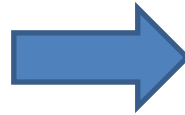


Moisture and ash content analysis

Methodology

Alteration of moisture content

- Addition of water to increase moisture content
- Mixing with dried sludge to lower moisture content



Rheometer:

- Static tests (flow)
- Dynamic tests (viscoelasticity)

Modelling

Power Law

$$\tau = K \cdot \dot{\gamma}^n \quad \left\{ \begin{array}{l} K = a \cdot MC^b \\ n = c \cdot MC^d \end{array} \right.$$

τ : shear stress [Pa]
 $\dot{\gamma}$: shear rate [s^{-1}]
 n : flow behaviour index [-]
 K : consistency coefficient

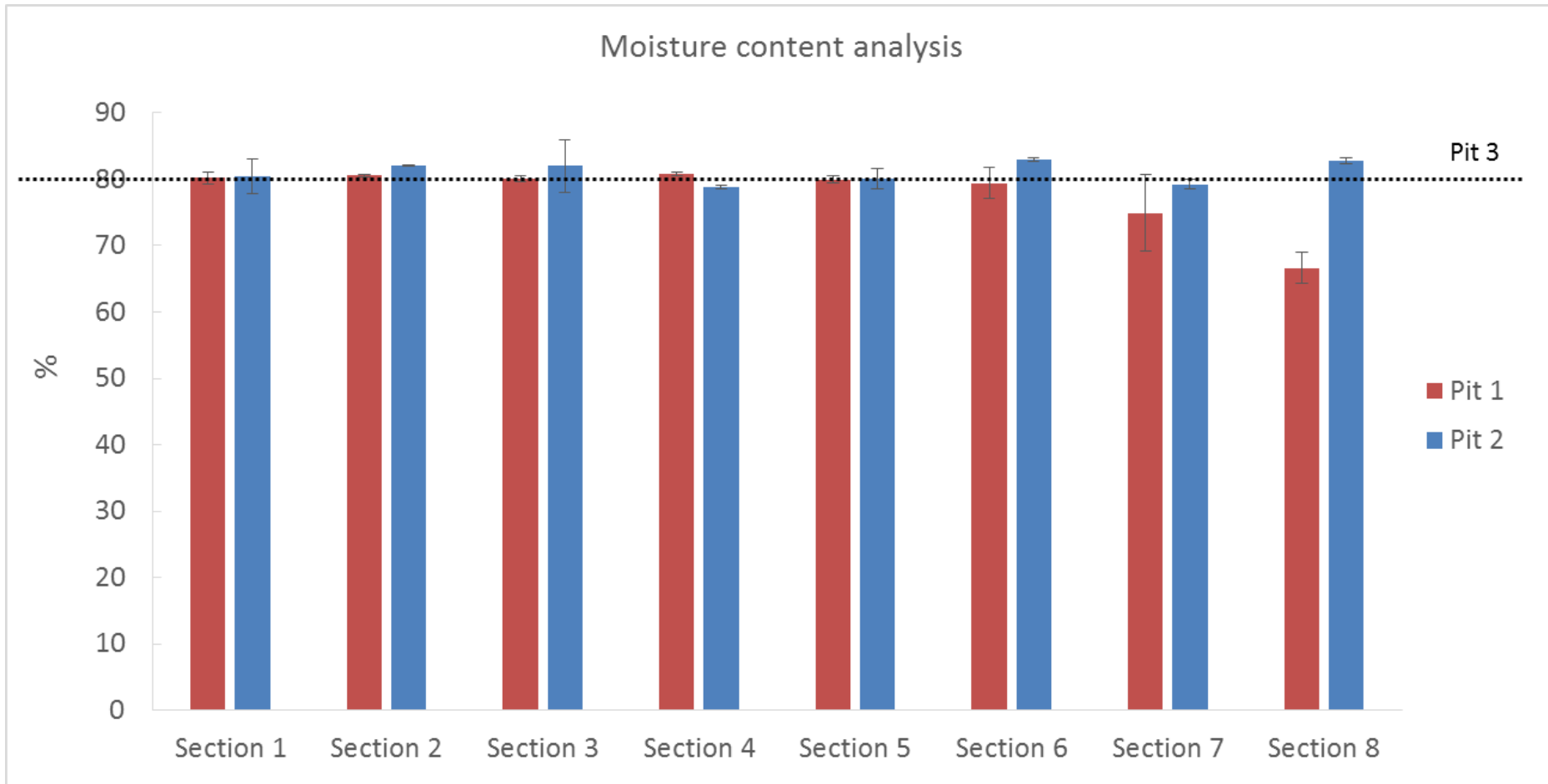
Application for pit emptying

$$\Delta P = \frac{4 \cdot \rho \cdot f \cdot L \cdot V^2}{2 \cdot D} \quad \left\{ \begin{array}{l} f = \frac{16}{Re'} \\ Re' = \frac{VD\rho}{K} \left(\frac{4n}{1+3n} \right)^n \left(\frac{D}{8V} \right)^{n-1} \\ V = \frac{Q}{\pi \cdot \left(\frac{D}{2} \right)^2} \end{array} \right.$$

V : average velocity [$m \cdot s^{-1}$]
 D : pipe diameter [m]
 L : pipe length [m]
 ρ_m : sludge density [$kg \cdot m^{-3}$]
 f : friction factor [-]
 Re' : power law modified
Reynolds number [-]
 ΔP : total frictional pressure
drop in the pipe [Pa]



Composition sludge

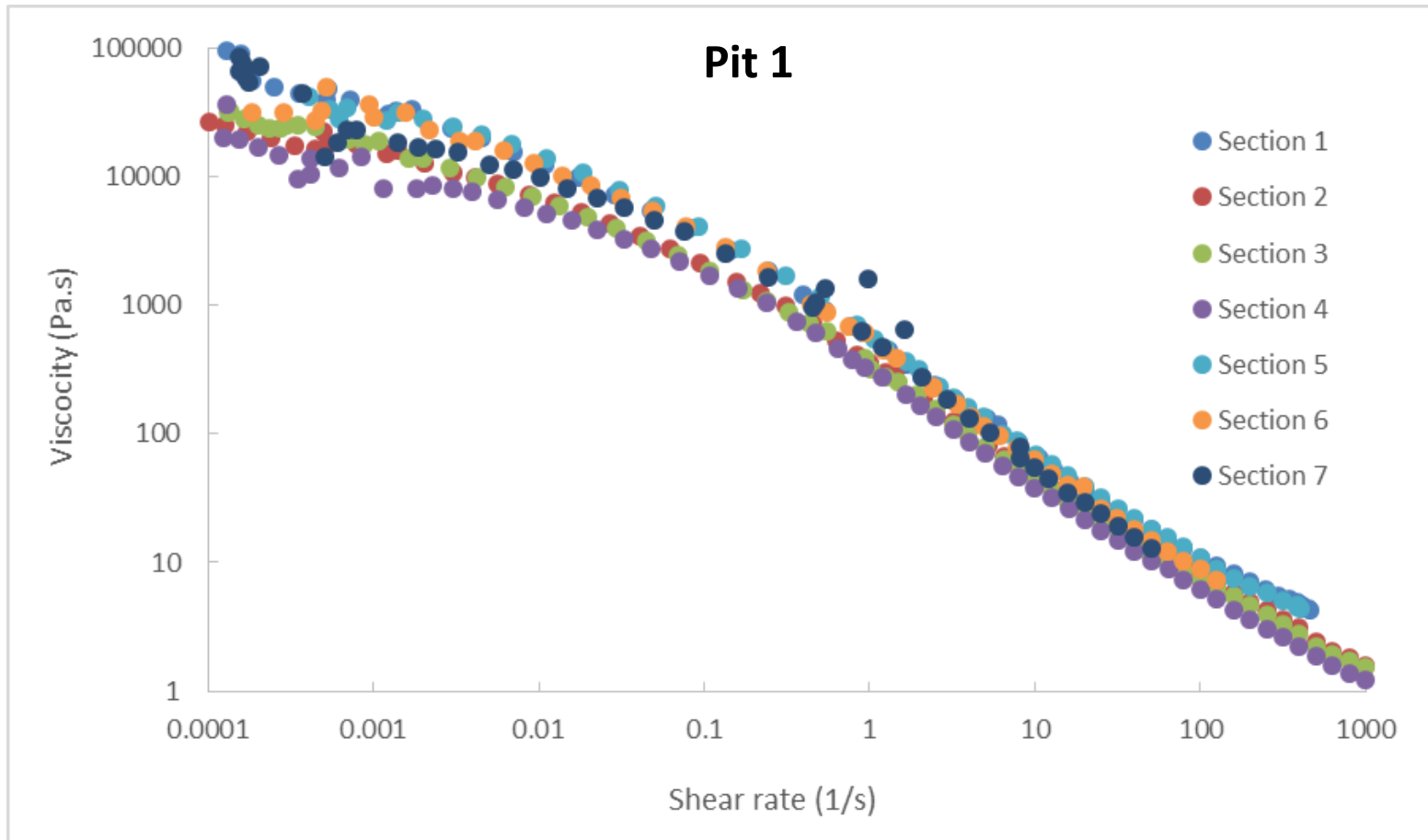


~ 80% moisture, except for section 8, pit 1 (~ 65%)

~ 35 % ash



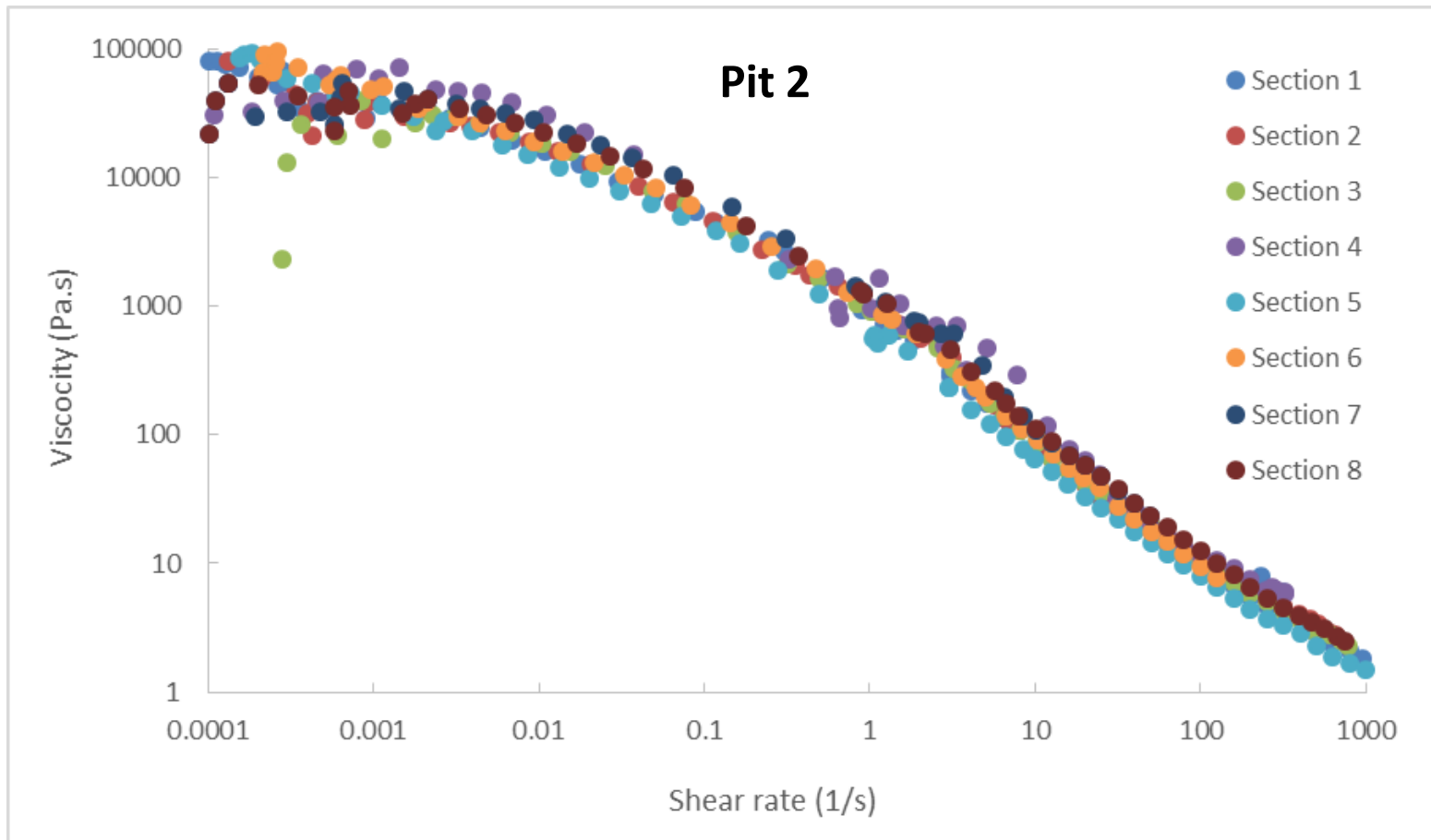
Viscosity - comparison between pit sections



Section 8: not possible to perform analysis
(no flow possible)



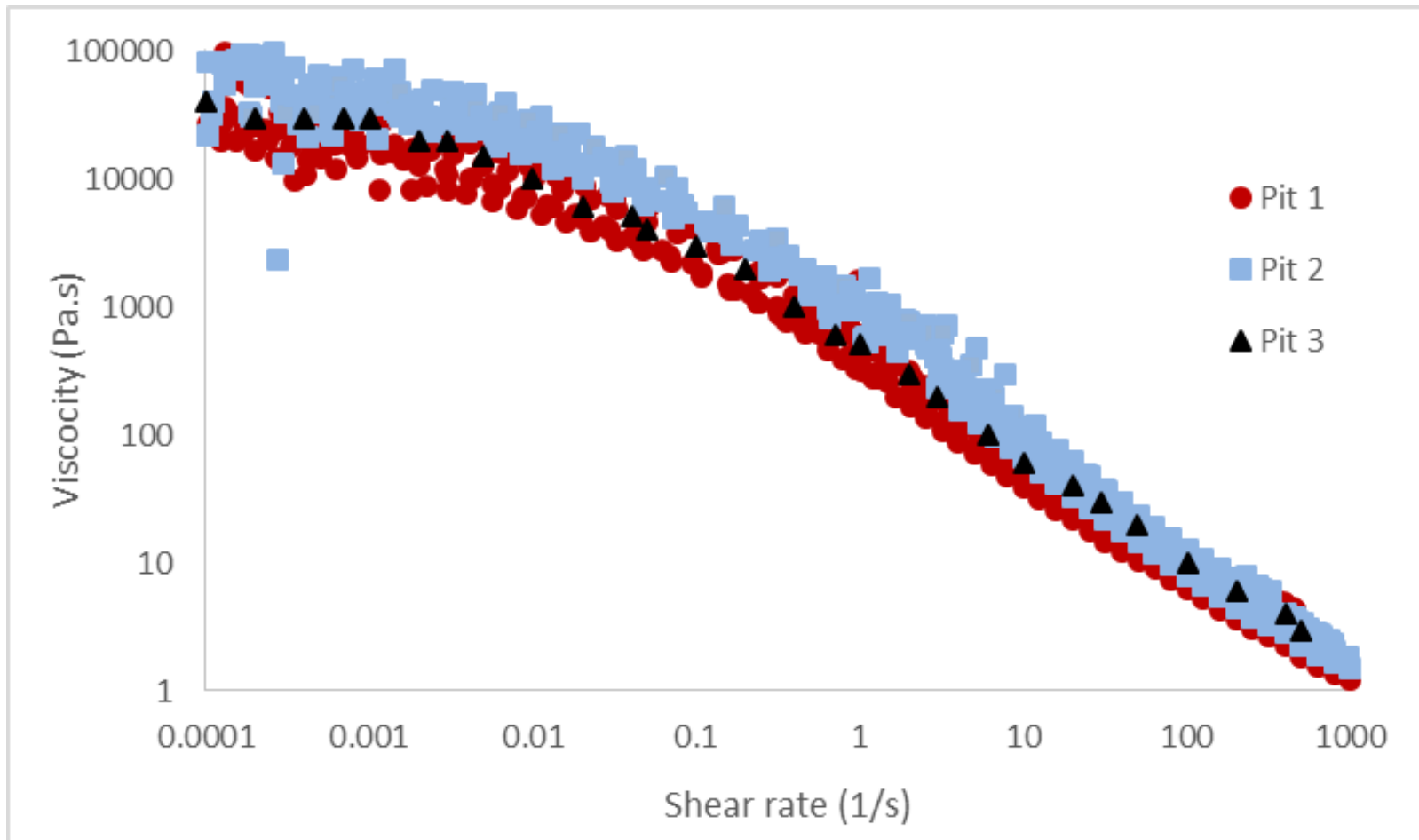
Viscosity - comparison between pit sections



**SHEAR THINNING BEHAVIOUR
NO EFFECT OF PIT SECTION**



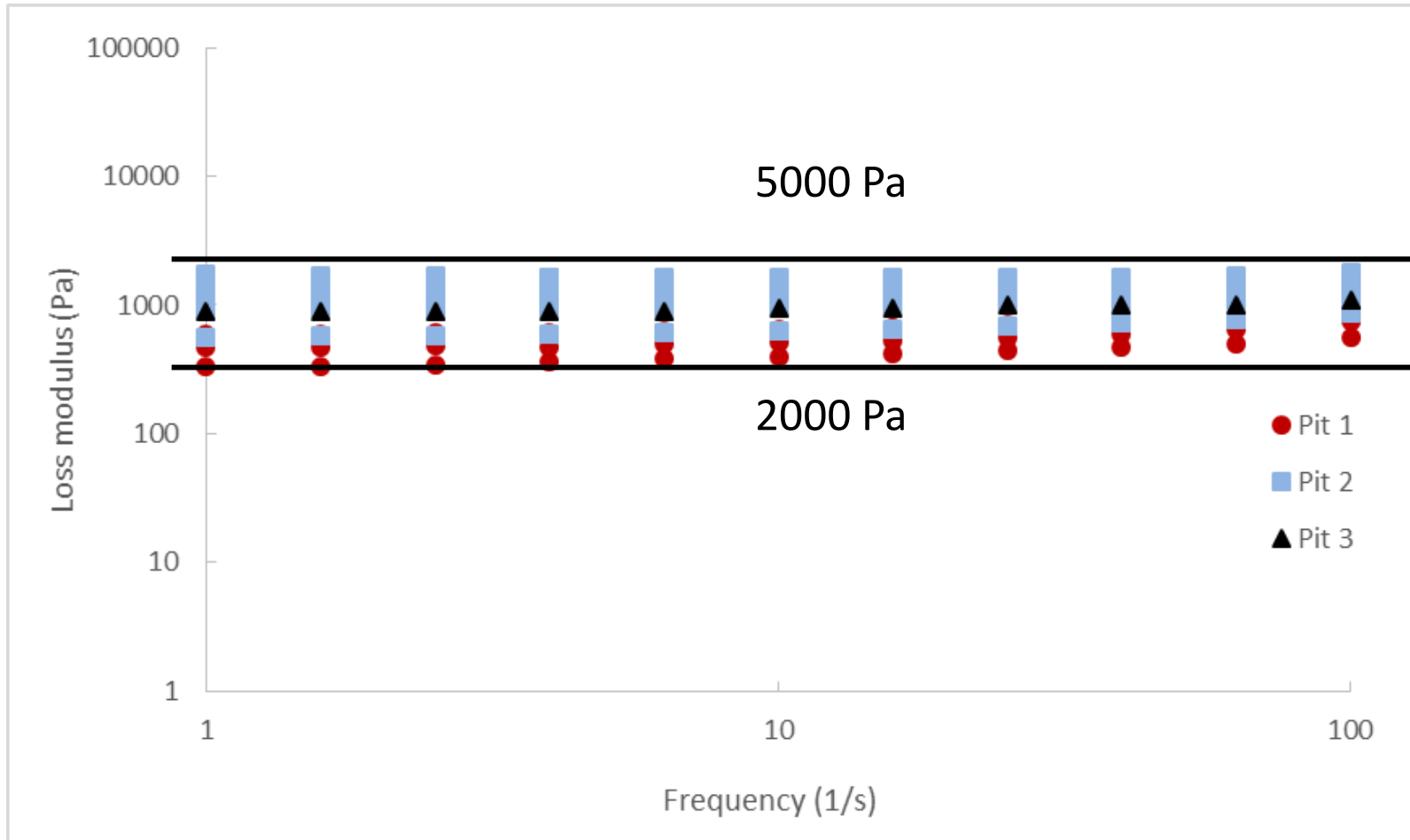
Viscosity - comparison between pits



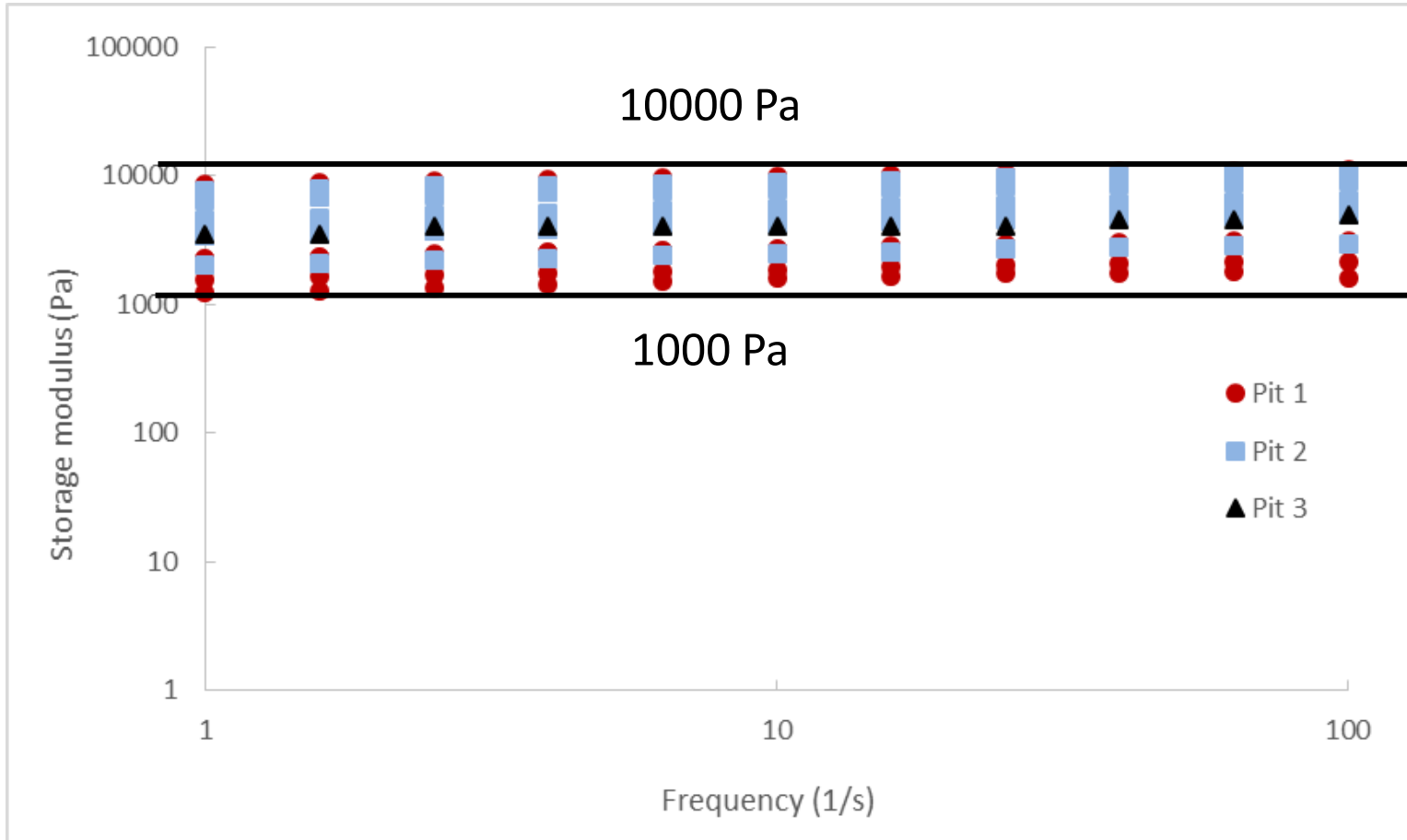
SAME BEHAVIOUR FOR DIFFERENT PITS



Viscoelastic properties



Viscoelastic properties



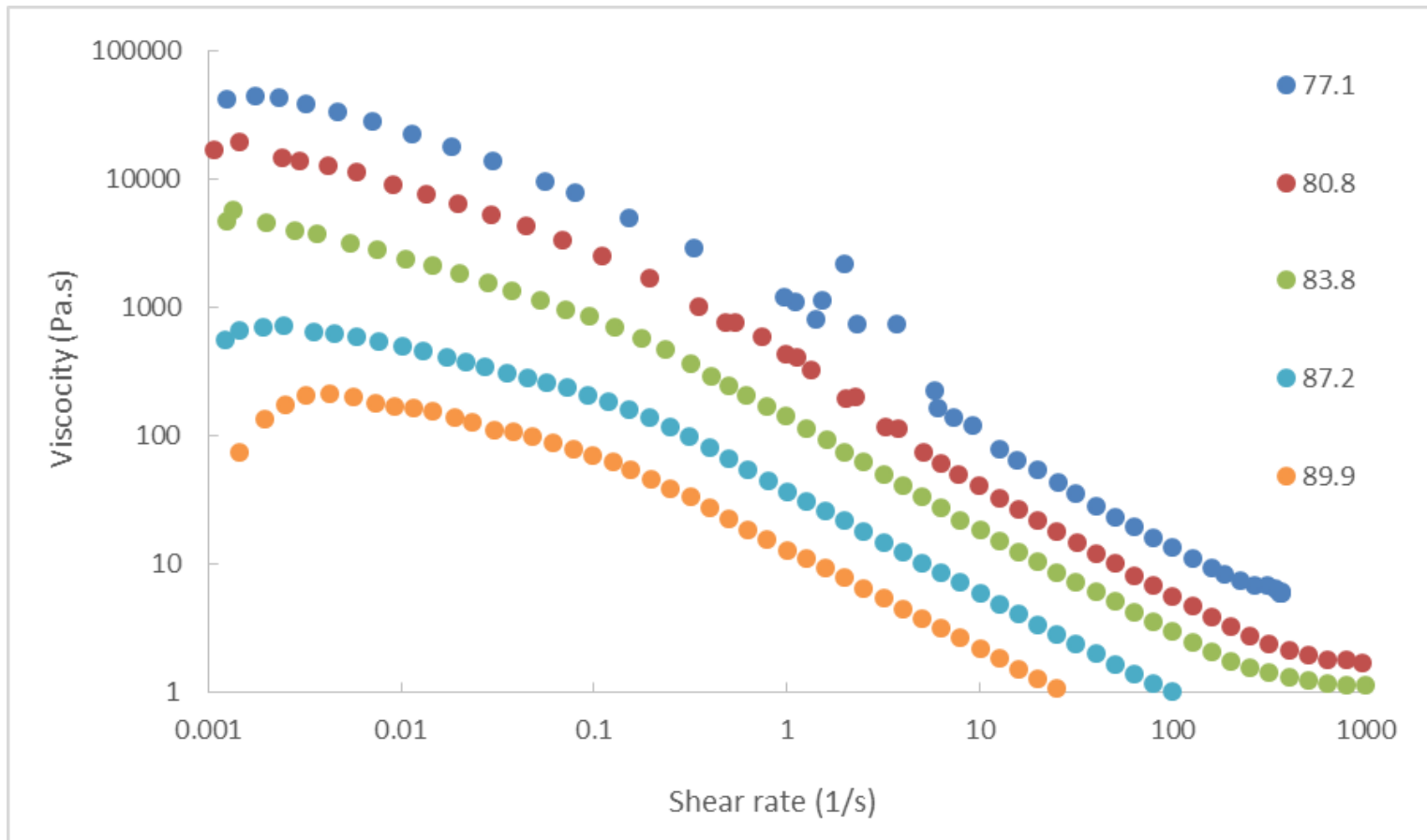
Viscoelastic properties

**Damping factor = Loss modulus /
Storage modulus < 1**

**ELASTICITY > VISCOCITY
YIELD STRESS FOR FLOW
(~1 – 20 Pa)**



Effect of moisture content of sludge



DECREASE OF MOISTURE CONTENT

→ DECREASE OF VISCOCITY



Effect of moisture content of sludge

Damping factor for different moisture contents < 1

DECREASE OF MOISTURE CONTENT

→ INCREASE DAMPING FACTOR

→ DECREASE OF YIELD STRESS ($< 1 \text{ Pa}$)



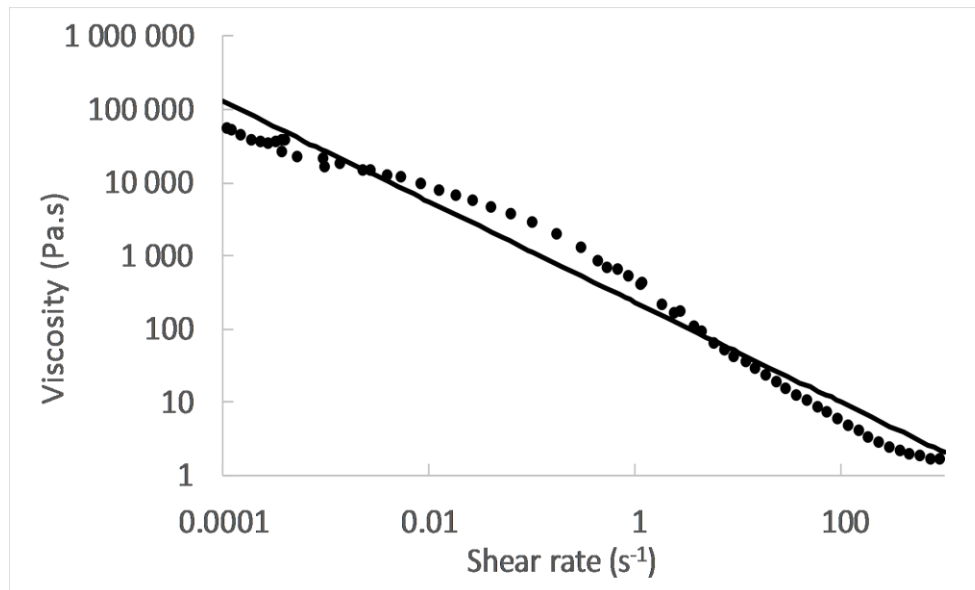
Modelling

Power Law

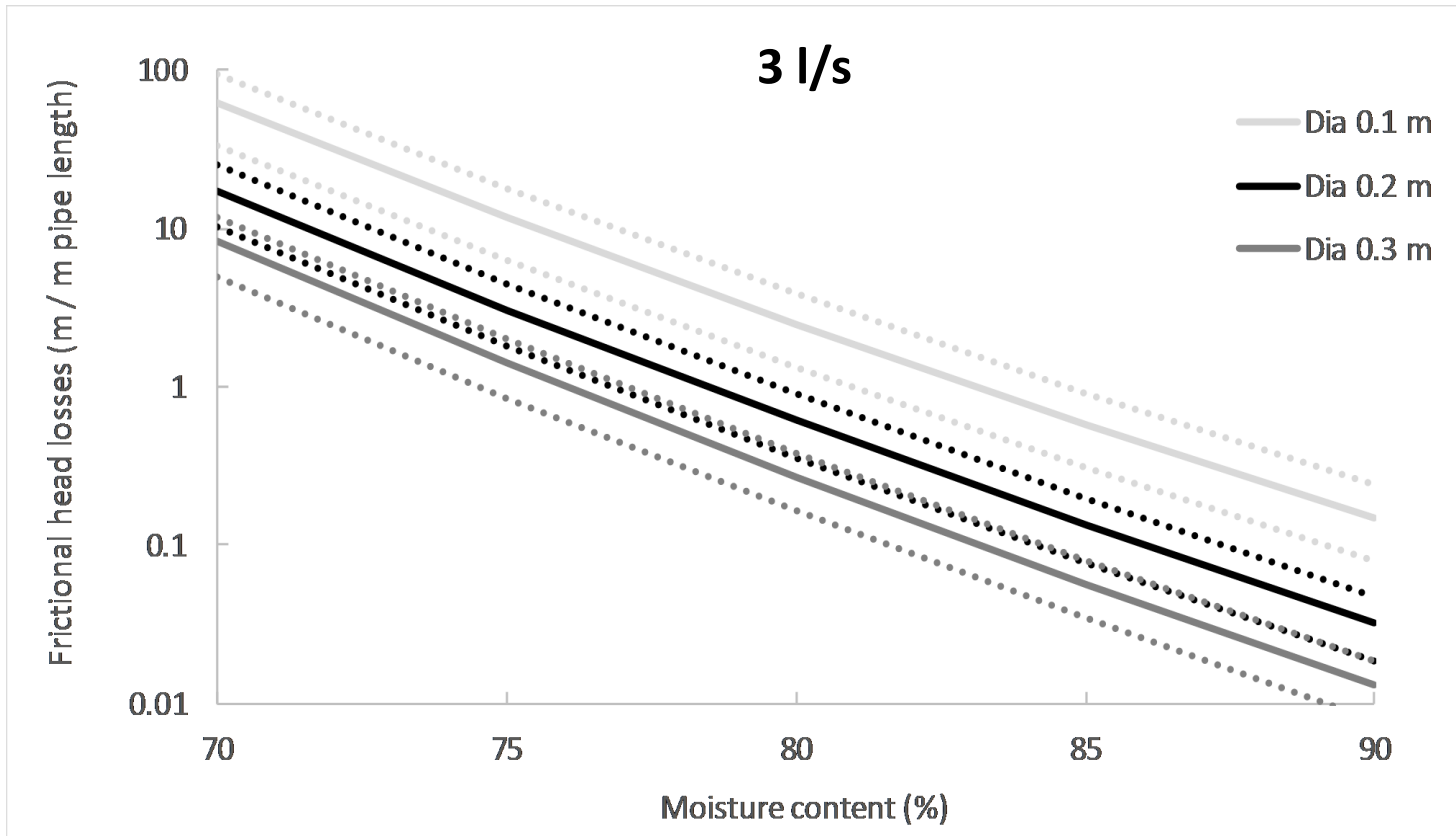
$$\tau = K \cdot \dot{\gamma}^n \quad \left\{ \begin{array}{l} K = 1.9 \times 10^{51} \cdot MC^{-25.7} \\ n = 3.2 \times 10^{-4} \cdot MC^{1.6} \end{array} \right. \quad \begin{array}{l} \text{Different from fresh faeces} \\ \text{(Wolley et al. (2014))} \end{array}$$

Average deviation of 13 and 5% for K and n , respectively

Maximum deviation of 37 and 9% for K and n , respectively



Pumping requirements



INCREASE OF PUMPABILITY

→ **INCREASE OF MOISTURE CONTENT**

→ **INCREASE OF PIPE DIAMETER**



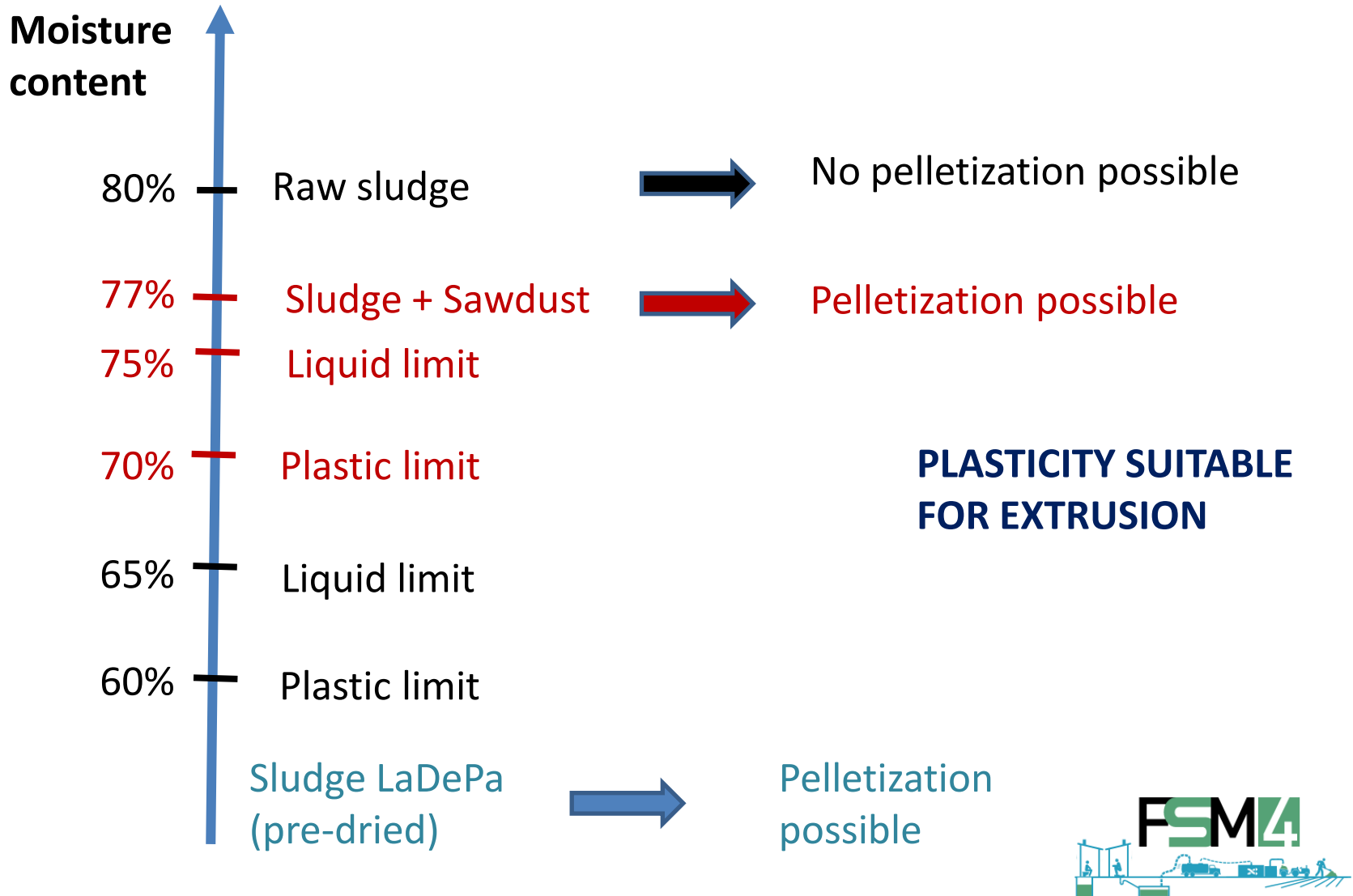
Pumping requirements

Omni-Ingestor criteria:

- Pit emptying rate = 3 l/s
- Pipe horizontal length = 100 m ; vertical length = 20 m

	Pipe diameter (m)	Moisture %			
		75	80	85	90
Hydraulic head (m)	0.2	924-2537	180 -479	52-115	27-42
	0.3	298-714	65 -133	28-41	22-24
Pressure (bar)	0.2	125-344	24-65	7.1-16	3.7-5.7
	0.3	40-97	8.8-18	3.8-6.0	2.9-3.3
Power (kW)	0.2	38-104	7.4-20	2.1-4.7	1.1-1.7
	0.3	12-29	2.7-5.5	1.2-1.7	0.9-1.0

Plasticity and extrusion



Conclusion about VIP faecal sludge

- ❑ Shear thinning fluid
- ❑ Elastic behaviour at rest → yield stress
- ❑ Similar rheological behaviour within the pit and among different latrines
- ❑ Low plasticity of sludge, so need to add a plasticiser (example: sawdust) or dewatering for extrusion
- ❑ Addition of water leading to the reduction of viscosity and yield stress → significant increase of pumpability

However: Addition of water not suitable depending on the upstream process (extrusion, drying)



Let's evolve to a safer pit emptying!



Thanks
a lot!



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